

DEVELOPMENT OF A PORT-STREAM BASED EQUATION ORIENTED MODELLING OF DIVIDING WALL COLUMN USING MOAIC

ROSSHILA BINTI IDRIS

Master of Science

UNIVERSITI MALAYSIA PAHANG



SUPERVISOR'S DECLARATION

We hereby declare that We have checked this thesis and in our opinions, this thesis is adequate in terms of scope and quality for the award of the degree of Master of Science.

(Supervisor's Signature)

Full Name : DR.-ING. MOHAMAD RIZZA BIN OTHMAN

Position : SENIOR LECTURER

Date :

(Co-supervisor's Signature)

Full Name : DR. NOORLISA HARUN

Position : SENIOR LECTURER

Date :



STUDENT'S DECLARATION

I hereby declare that the work in this thesis is based on my original work except for quotations and citations which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at Universiti Malaysia Pahang or any other institutions.

(Student's Signature)

Full Name : ROSSHILA BINTI IDRIS

ID Number : MKC15037

Date :

DEVELOPMENT OF A PORT-STREAM BASED EQUATION ORIENTED
MODELLING OF DIVIDING WALL COLUMN USING MOSAIC

ROSSHILA BINTI IDRIS

Thesis submitted in fulfillment of the requirements
for the award of the degree of
Master of Science

Faculty of Chemical & Natural Resources Engineering
UNIVERSITI MALAYSIA PAHANG

FEBRUARY 2019

ACKNOWLEDGEMENTS

I would like to express my sincere gratitude to my main supervisor Dr.-Ing. Mohamad Rizza Othman who had been guiding and supporting me throughout my research with full of motivation, enthusiasm, and knowledge.

I also would like to express my sincere appreciation to my co-supervisor Dr. Noorlisa Harun for her willingness and guidance in tutoring me for this research.

Furthermore, appreciation to the Malaysia Ministry of Education under grant no. RDU140105 and RDU1603148 for supporting this research work.

Last but not least, special thanks dedicated to my parents for their endless love, support, prayers, and sacrifice.

ABSTRAK

Lajur dinding pembahagian (DWC) dianggap sebagai lajur penyulingan bukan standard yang rumit. Konfigurasi bahagian yang berbeza dalam DWC dibahagikan dengan dinding menegak di dalam ruang meningkatkan kerumitan pemodelan DWC disebabkan kewujudan gelung kitar semula atau aliran yang saling berkaitan. Kaedah yang berorientasikan persamaan (EO) sangat sesuai untuk menangani masalah seperti itu berbanding dengan pendekatan modular berurutan (SM) yang sering membawa kepada masalah penumpuan. Pada tahap yang sangat asas, pendekatan pemodelan DWC perlu dipercayai untuk dilanjutkan sepenuhnya kepada aplikasi lanjutan lain seperti kawalan proses dan pengoptimuman. Dalam makalah ini, pendekatan pemodelan sistematik bagi keadaan mantap DWC dibentangkan yang merangkumi sambungan dan port unit sambungan yang boleh diterima untuk aliran data EO menggunakan MOSAIC. MOSAIC adalah persekitaran pemodelan berasaskan web baru yang direka untuk meminimumkan kesilapan pemodelan, mengurangkan usaha dan kesilapan pengaturcaraan, meningkatkan dokumentasi fail, galakan penyimpanan data koperasi dan perkongsian dan penggunaan semula model dan bahagian model terutamanya untuk pemodelan proses kimia. Pendekatan sedemikian menunjukkan set sistem persamaan yang secara fungsional seperti operasi unit, dengan adanya pelabuan dan kewujudan aliran dalam menyambungkan semua sistem persamaan bersama-sama. Melalui pendekatan ini, bahagian-bahagian DWC yang berlainan boleh digabungkan sebagai satu lajur dalam satu helaian lajur. Untuk menguji fungsi pendekatan yang dicadangkan, satu kajian kes dengan dua set data eksperimen yang berbeza dipertimbangkan iaitu pemisahan metanol / 1-propanol / 1-butanol. Kemudian model yang dibangunkan digunakan untuk fraksionasi Asid Fatty (FA) untuk memisahkan cahaya (LC), potong tengah (MC), dan potongan berat (HC). Kedua-dua model menunjukkan penumpuan yang baik dengan ralat yang boleh diterima yang membuktikan kesahan pembangunan model. Untuk melanjutkan fungsian model, kajian selanjutnya telah dijalankan untuk menguji analisis interaksi antara pembolehubah yang dimanipulasi (MV) dan pembolehubah terkawal (CV) pada DWC untuk merekabentuk dan mencadangkan konfigurasi kawalan yang sesuai menggunakan analisis nilai tunggal (SVA) dan array gain relatif (RGA).

ABSTRACT

Dividing wall column (DWC) is considered as a complex non-standard distillation column. The different sections configurations within the DWC divided by the vertical wall inside the column increase the complexity of modelling DWC due to the existence of recycle loops or interconnecting streams. An equation-oriented (EO) approach is well suited to handle such problem compared to sequential modular (SM) approach which often leads to convergence problems. At a very basic level, the modelling approach of DWC needs to be reliable to be fully extended to other advanced applications such as process control and optimization. In this paper, a systematic modelling approach of steady-state DWC is presented which encompasses ports and stream unit connectivity that is admissible to EO process flowsheet using MOSAIC. MOSAIC is a new web-based modelling environment which is designed to minimize modelling efforts, minimizing programming efforts, and as a code generator for many programming languages. Such approach present sets of equation system which functionally like a unit operation, with a presence of ports and the existence of streams in connecting all equation systems together. Some adjustment on equations involved has been made accordingly to suit with the port and stream connectivity features particularly in interconnecting streams (liquid and vapour split). Through this approach, different sections of DWC can be combined as a single column in a flowsheet. To test the functionality of the proposed approach, a case study with two different experimental data set were considered which is the separation of methanol/ 1-propanol/ 1-butanol. Then the developed model is applied for the Fatty Acid (FA) fractionation to separate the light-cut (LC), middle-cut (MC), and heavy-cut (HC). Both models show good convergence with an acceptable error below than 10% which proves the validity of the model development.

TABLE OF CONTENT

DECLARATION	
TITLE PAGE	
ACKNOWLEDGEMENTS	ii
ABSTRAK	iii
ABSTRACT	iv
TABLE OF CONTENT	v
LIST OF TABLES	viii
LIST OF FIGURES	ix
LIST OF SYMBOLS	xi
LIST OF ABBREVIATIONS	xiii
CHAPTER 1 INTRODUCTION	1
1.1 Dividing Wall Column Background	1
1.2 Problem statement	4
1.3 Research contributions	6
1.4 Objective	7
1.5 Scopes	7
1.6 Overview of Thesis	7
CHAPTER 2 LITERATURE REVIEW	9
2.1 Introduction	9
2.2 Modelling and simulation approach of Process Model	9
2.2.1 Sequential Modular (SM) approach in Modelling DWC	12

2.2.2	Equation Oriented (EO) Approach in Modelling DWC	15
2.3	MOSAIC Modelling Software	16
2.4	Process flowsheet in MOSAIC	18
2.4.1	Unit Block Model	18
2.5	Modelling of Dividing Wall Column	19
2.5.1	Equation System and Variables for DWC	20
2.6	Summary	24
CHAPTER 3	METHODOLOGY	25
3.1	Introduction	25
3.2	Adjustment of DWC Internal Connection Equations Structure	25
3.3	Defining Unit by Adding Ports	29
3.3.1	Standardizing the Input and Output Variables Through Interface	36
3.4	Unit block connectivity using Streams	38
3.5	Model development in MOSAIC	40
3.5.1	Define Notation of Variables	40
3.5.2	Creating the Equations and Equation Systems	41
3.5.3	Equation System as Unit Operation	43
3.5.4	Connecting two different ports using streams	45
3.6	Model solving of DWC	47
3.6.1	Equation System of DWC in MOSAIC	47
3.6.2	Setting the Index in the DWC Equation System	48
3.6.3	Variable Specification in MOSAC	49
3.6.4	Code Generation in MOSAIC	49
3.7	Model Case Studies	50

3.7.1	Case Study 1: Separation of Ternary Mixture: Methanol/ 1-Propanol/ 1-Butanol	50
3.7.2	Case Study 2: Fatty Acid fractionation	52
3.8	Summary	54
CHAPTER 4 RESULTS AND DISCUSSION		55
4.1	Introduction	55
4.2	The substitution of interface variable with variables in the equation system of unit block	55
4.3	The degree of Freedom Structure Analysis	61
4.4	Initialization Value	67
4.5	Model Solver	67
4.6	Model Validation and Analysis	68
4.6.1	Case Study 1: Separation of Ternary Mixture: Methanol/ 1-Propanol/ 1-Butanol	68
4.6.2	Case Study 2: Fatty Acid fractionation	70
4.7	Summary	73
CHAPTER 5 CONCLUSION		74
5.1	Introduction	74
5.2	Recommendation	75
REFERENCES		76
APPENDIX A		81
APPENDIX B		82
APPENDIX C		89

LIST OF TABLES

Table 2.1	Previous studies of DWC EO modelling (based on programming language)	16
Table 3.1	Equation system of condenser unit block	30
Table 3.2	Equation system of rectifying unit block	30
Table 3.3	Equation system of Pre-fractionator unit block	30
Table 3.4	Equation system of Main unit block	31
Table 3.5	Equation system of stripping unit block	31
Table 3.6	Equation system of reboiler unit block	32
Table 3.7	Variables in equation system and its interface variables	37
Table 3.8	The name space of each unit block with ports	37
Table 3.9	Number of streams with its connected elements	38
Table 3.10	Operating parameter of alcohol ternary mixture for the 1 st data set	51
Table 3.11	Operating parameter of alcohol ternary mixture for the 2 nd data set	52
Table 3.12	Design parameter of Fatty Acid mixture	54
Table 4.1	Substitution of interface variables with streams in the condenser equation system	57
Table 4.2	Substitution of interface variables with streams in the rectifying equation system	57
Table 4.3	Substitution of interface variables with streams in the pre-fractionator equation system	58
Table 4.4	Substitution of interface variables with streams in the main equation system	59
Table 4.5	Substitution of interface variables with streams in the stripping equation system	60
Table 4.6	Substitution of interface variables with streams in the reboiler equation system	61
Table 4.7	Variable specification of DWC equation systems	62
Table 4.8	Well-determined DOF of DWC equation system	64
Table 4.9	Comparison with 1 st set of experimental data	68
Table 4.10	Comparison with the 2 nd set of experimental data	69
Table 4.11	Comparison between specified product value in Aspen Plus and EO simulation.	70

LIST OF FIGURES

Figure 1.1	Direct (a) and indirect (b) sequence of the conventional distillation column	2
Figure 1.2	Petlyuk column	2
Figure 1.3	Dividing wall column (DWC) configuration	3
Figure 2.1	A process flowsheet	10
Figure 2.2	A simulation flowsheet	10
Figure 2.3	Simulation of the DWC system using two columns sequence	12
Figure 2.4	Four columns sequence	13
Figure 2.5	Implementation four configuration of DWC in aspen dynamics	14
Figure 2.6	Symbolic expression in MOSAIC	17
Figure 2.7	Equation system that represents unit with ports	18
Figure 2.8	Connection via internal streams of two units block having ports	19
Figure 2.9	Four divided sections in DWC	19
Figure 3.1	Internal stream of DWC	26
Figure 3.2	DWC is treated as six unit blocks in MOSAIC	29
Figure 3.3	Input and output ports in condenser and rectifying unit block	32
Figure 3.4	Input and output ports at the intersection of rectifying (upper), pre-fractionator (left), and main (right) unit block.	33
Figure 3.5	Input and output ports at the intersection of stripping (bottom), pre-fractionator (left), and main (right) unit block	35
Figure 3.6	Input and output ports in stripping (bottom) and reboiler unit block	36
Figure 3.7	Port and interface application in DWC	38
Figure 3.8	Complete schematic model of DWC with ports and streams application in MOSAIC	39
Figure 3.9	The flow chart of developing DWC model using MOSAIC	40
Figure 3.10	Notation declaration	41
Figure 3.11	Mathematical equation expression in MOSAIC	42
Figure 3.12	Equation system editor of connected elements/equations	42
Figure 3.13	List of new variable names in the interface	43
Figure 3.14	Matching elements in MOSAIC	44
Figure 3.15	Creating new equation system for each unit block	45
Figure 3.16	Adding ports to the new equation system (equation system equipped with ports)	45
Figure 3.17	Flowsheet equation system	46
Figure 3.18	Adding stream into the equation systems	46

Figure 3.19	Connected elements in the stream	47
Figure 3.20	Developed model with completed streams connection	47
Figure 3.21	Hierarchical equation system of DWC	48
Figure 3.22	Index specification of each unit block in DWC	48
Figure 3.23	Variables specification in MOSAIC	49
Figure 3.24	Exported DWC model coding in gProms	50
Figure 3.25	Schematic of DWC pilot plant (1 st data set)	51
Figure 3.26	Schematic of DWC pilot plant and input parameter (2 nd data set)	52
Figure 3.27	Schematic DWC configuration for fatty acid fractionation	53
Figure 4.1	Schematic model of DWC flowsheet	56
Figure 4.2	Unstable structure analysis of DWC system	63
Figure 4.3	Well determined structure analysis of DWC system	65
Figure 4.4	Symbolic mathematical expression of variable specifications in MOSAIC	66
Figure 4.5	Elements involved in DWC evaluation model	67
Figure 4.6	(a) Light-cut, (b) middle-cut, and (c) heavy-cut composition trend in DWC column	72

LIST OF SYMBOLS

H	Enthalpy
P	Pressure
Q	Heat duty
K	Equilibrium constant/ Open loop gain matrix
D	Distillate flowrate
B	Bottom flowrate
S	Side flowrate
F	Side flowrate
V	Vapour flow /vapour boil-up
L	Liquid flow
c	Interface variable for vapour/liquid composition
f	Interface variable for vapour/liquid flowrate
z	Feed composition
y	Vapour composition/ mole fraction
x	Liquid composition/ mole fraction
α	Liquid split factor
β	Vapour split factor
γ	Activity coefficient

Superscript

V	Vapour
L	Liquid
F	Feed
O	Saturated vapour
D	Distillate
R	Reboiler
$bottom$	Stripping section
$upper$	Rectifying section
$left$	Pre-fractionator section
$right$	Main section
$distillate$	Distillate stream product

<i>middle</i>	Middle side stream
<i>in</i>	Flow in
<i>out</i>	Flow out

Subscript

<i>j</i>	j^{th} stage/ controlled variable in RGA
<i>i</i>	j^{th} component/ manipulated variable RGA
<i>k</i>	Interface variable for vapour/liquid composition of component i
<i>o</i>	Reflux rate
<i>D</i>	Distillate
<i>c</i>	Condenser
<i>R</i>	Reboiler
<i>L</i>	Liquid
<i>V</i>	Vapour
<i>W</i>	Bottom

LIST OF ABBREVIATIONS

ACM	Aspen Custom Modeler
AMPL	A Mathematical Programming Language
BDNSOL	Block Decomposition Non-Linear Solver
C++	General Purpose Programming Language
DAEs	Differential Algebraic Equations
DOF	Degree of Freedom
DWC	Dividing Wall Column
EO	Equation Oriented
ES	Equation System
FA	Fatty Acid
Fortran	Formula Translation
FUGK	Fenske-Underwood-Gilliland-Kirkbride
GAMS	General Algebraic Modelling System
gPROMS	General Process Modelling System
GUI	Graphical User Interface
HC	Heavy Cut Component of Fatty Acid Fractionation
LaTeX	Text Document
LC	Light Cut Component of Fatty Acid Fractionation
MathML	Mathematical Markup Language
MESH	Material, Equilibrium, Summation, Heat
MC	Middle Cut Component of Fatty Acid Fractionation
MIMO	Multiple-Input Multiple-Output
MOSAIC	Model Specification on Documentation Level
NLE	Non-Linear Equation System
NDOF	Number degree of freedom
NEQN	Number of equations
NFIX	Number of fixed variables
NSPEC	Net specifications
NVAR	Number of variables
OCM	Oxidative Coupling of Methane
ODE	Ordinary Differential Equations

RADFRAC	ASPEN's Rigorous Distillation Method
RGA	Relative Gain Array
SCILAB	Numerically Oriented Programming Language
SISO	Single-Input Single-Output
SM	Sequential Modular
SPARSE	Newton-Type Method Without Block Decomposition

REFERENCES

- Aspen Technology, I. (2004). *Getting Started Using Equation Oriented Modeling*. Cambridge.
- Bristol, E. (1966). On a new measure of interaction for multivariable process control. *IEEE Transactions on Automatic Control*, 11(1), 133–134.
- Canter, D. L. (1987). A Detailed Steady-State Control Analysis of an Ethanol-Water Distillation Column.
- Chansomwong, A., Zanganeh, K. E., Shafeen, A., Douglas, P. L., Croiset, E., & Ricardez-Sandoval, L. A. (2011). A decentralized control structure for a CO₂compression, capture and purification process: An uncertain Relative Gain Array approach. *In World Congress* (Vol. 18, No.1, pp. 8558-8563)
- Cho, Y., Kim, B., Kim, D., Han, M., & Lee, M. (2009). Operation of divided wall column with vapor sidedraw using profile position control. *Journal of Process Control*, 19(6), 932–941.
- Dejanovic, I., Matijasevic, L., & Olujic, Z. (2010). Dividing wall column-A breakthrough towards sustainable distilling. *Chemical Engineering and Processing: Process Intensification*, 49(6), 559–580.
- Dimian, A. C., Bildea, C. S., & Kiss, A. A. (2014). *Integrated Design and Simulation of Chemical Processes* (Vol. Volume 13). USA: Elsevier.
- Dohare, R. K., Singh, K., & Kumar, R. (2015). Modeling and model predictive control of dividing wall column for separation of Benzene–Toluene- *o* -Xylene. *Systems Science & Control Engineering*, 3(1), 142–153.
- Edna, A., Ignacio, S. L., Gabriel, J., Hern, S. S., Segovia-hernandez, J. G., & Hern, S. (2016). Rigorous Modeling, Simulation and Optimization of a Conventional and Nonconventional Batch Reactive Distillation Column: a comparative study of dynamic optimization approaches. *Chemical Engineering Research and Design*, 111, 83-99.
- Gani, R., Cameron, I. T., Lucia, A., Sin, G., & Georgiadis, M. (2012). Process Systems Engineering, 2. Modeling and Simulation. *Ullmann's Encyclopedia of Industrial Chemistry*.

- Halvorsen, I. J., & Skogestad, S. (2001). Distillation Theory. *Encyclopedia of Separation Science* (pp. 1117–11134).
- Hanratty, P. J., & Myers, J. E. (2004). Exploiting the Use of Equation-Oriented Modeling for Design-Type Problems. In *Conference on Foundations of Computer-Aided Process Design* (pp. 299–302). Princeton, NJ.
- Hensen, W. (2005). Embedding equation oriented models of process unit operations in a sequential modular flowsheet simulator Study with a gas separation membrane model.
- Hiller, C., Buck, C., Ehlers, C., & Fieg, G. (2010). Nonequilibrium stage modelling of dividing wall columns and experimental validation. *Heat and mass transfer*, 46(10), 1209–1220.
- Ignat, R., & Woinaroschy, A. (2011). Dynamic Analysis and Controllability of Dividing- Wall Distillation Columns using a Four Points Control Structure. *Sci. Bull. Univ. "Politeh." Burcharest, Ser. B*, 73, 71.
- Illner, M., & Othman, M. R. (2014). Modelling and Simulation of a Dividing Wall Column for Separation of Fatty Acid in Oleochemical Industries. *Chemical Engineering Transactions*, 45, 925-930.
- Isopescu, R., Woinaroschy, A., & Draghiciu, L. (2008). Energy Reduction in a Divided Wall Distillation Column. *Revista de Chimie*, 59(1), 812–815.
- Kader, M. A. (2009). *The modelling and control of a 1-octane dividing wall distillation column*. Ph.D. Thesis. University of KwaZulu-Natal, Durban.
- Kiss, A. a., & van Diggelen, R. C. (2010). Comparison of Control Strategies for Dividing-Wall Columns. *Industrial & Engineering Chemistry Research*, 49, 288–307.
- Koko, I. O. M., & Barakat, T. A. M. (2015). Modelling and Control Analysis of Dividing Wall Distillation Columns. *University Of Khartoum Engineering Journal*, 5(1), 18–25.
- Kuntsche, S. (2011). MOSAIC User Guide, 1–64.
- Kuntsche, S., Barz, T., Kraus, R., Arellano-Garcia, H., & Wozny, G. (2011a). MOSAIC a web-based modeling environment for code generation. *Computers & Chemical Engineering*, 35(11), 2257–2273.

- Lam, C. P., Li, H., & Xu, D. (2007). A model-centric approach for the management of model evolution in chemical process modelling. *Computers & Chemical Engineering*, 31(12), 1633–1662.
- Ling, H., & Luyben, W. L. (2009). New control structure for divided-wall Columns. *Industrial and Engineering Chemistry Research*, 48(13), 6034–6049.
- Luyben, W. L. (1987). Sensitivity of Distillation Relative Gain Arrays to Steady-State Gains. *Industrial & Engineering Chemistry Research*, 26(10), 2076–2078.
- Mangold, M., Motz, S., & Gilles, E. D. (2002). A network theory for the structured modelling of chemical processes. *Chemical Engineering science*, 57(19), 4099–4116.
- Marchetti, M., Rao, A., & Vickery, D. (2001). Mixed mode simulation - Adding equation oriented convergence to a sequential modular simulation tool. In *Computer Aided Chemical Engineering*, (Vol. 9. pp. 231–236). Elsevier.
- Megan Jobson. (2005). Dividing wall distillation comes of age. *Chemical Engineer*, (766), 30-31.
- Moore, C. (1986). Application of Singular Value Decomposition to the Design, Analysis, and Control of Industrial Processes. In *In American Control Conference*, (pp. 643–650). IEEE.
- Mutalib, M. I. A., & Smith, R. (1998). Operation and Control of Dividing Wall Distillation Columns: Part 1: Degrees of freedom and dynamic simulation. *Chemical Engineering Research and Design*, 76(3), 308-318.
- Nelson, L., & Taylor, R. (2009). Modeling of Energy Efficient Dividing-Wall Distillation Columns. *Annual Symposium on undergraduate Research Experience*, 110.
- Nguyen, T. D., Rouzineau, D., Meyer, M., & Meyer, X. (2016). Design and simulation of divided wall column: Experimental validation and sensitivity analysis. *Chemical Engineering and Processing: Process Intensification*, 104, 94–111.
- Pantelides, C. C., Nauta, M., Matzopoulos, M., & Grove, H. (2015). Equation-Oriented Process Modelling Technology : Recent Advances & Current Perspectives. In *5th Annual TRC-Idemitsu Workshop*, 91.

- Pattison, R. C., Gupta, A. M., & Baldea, M. (2015). Equation-Oriented Optimization of Process Flowsheets with Dividing-Wall Columns. *AIChE Journal*, 62(3), 704-716.
- Piela, P. C., & Westerberg, A. W. (1994). *Equational-based Process Modeling* (pp. 1-76). Technical report, Department of Chemical Engineering and the Engineering Design Research Centre- Carnegie Mellon University, Pittsburgh.
- Rodrigues, A. E., & Minceva, M. (2005). Modelling and simulation in chemical engineering : Tools for process innovation. *Computers and Chemical Engineering*, 29(6), 1167-1183.
- Sankaranarayanan, D., & Deepakkumar, G. (2015). Implementing the Concept of Relative Gain Array for the Control of MIMO System : Applied To Distillation Column. *International Journal of Advanced Research in Electrical, Electronic and Instrumentation Engineering*, 4(5), 4648-4653.
- Schultz, M. A., Stewart, D. G., Harris, J. M., Rosenblum, S. P., Shakur, M. S., & O'Brien, D. E. (2002). Reduce costs with dividing-wall columns. *Chemical Engineering Progress*, 98(5), 64-71.
- Shacham, M., Macchietto, S., Stutzman, L. F., & Babcock, P. (1982). Equation oriented approach to process flowsheeting. *Computers & Chemical Engineering*, 6(2), 79-95.
- Staak, D., Grützner, T., Schwegler, B., & Roederer, D. (2014). Dividing wall column for industrial multi purpose use. *Chemical Engineering and Processing: Process Intensification*, 75(January), 48-57.
- Strandberg, J. . (2011). *Optimal operation of divided wall column*. Norwegian University of Science and Technology.
- Van Diggelen, R. C. (2007). *Multivariable feedback control of a Dividing Wall Column*. Doctoral dissertation, Delft University of Technology.
- Varma, G. V., Lau, K. H., & Ulrichson, D. L. (1993). A new tearing algorithm for process flowsheeting. *Computers and Chemical Engineering*, 17(4), 355-360.
- Wang, S., & Wong, D. S. H. (2007). Controllability and energy efficiency of a high-purity divided wall column. *Chemical Engineering Science*, 62(4), 1010-1025.

- Wolff, E., & Skogestad, S. (1995). Operation of integrated three-product (Petlyuk) distillation columns. *Industrial & Engineering Chemistry Research*, 34(6), 2094–2103.
- Wright, R. O. (1949). *U.S. Patent No. 2,471,134*. Washington, DC: U.S. Patent and Trademark Office.
- Yildirim, Ö., Kiss, A. A., & Kenig, E. Y. (2011). Dividing wall columns in chemical process industry: A review on current activities. *Separation and Purification Technology*, 80(3), 403–417.